

5                   **USE OF A THERMOPLASTIC VULCANIZATE AS AN IMPACT  
MODIFIER IN BLENDS OF POLYESTER AND POLYCARBONATE**

Claim of Priority

                  This application claims priority from U.S. Provisional Patent  
Application Serial Number 60/536,012 bearing Attorney Docket Number  
10   12003019 and filed on January 13, 2004.

Field of the Invention

                  This invention relates the use of a thermoplastic vulcanizate as an impact  
modifier in blends of polyester and polycarbonate.

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Background of the Invention

                  Blends of polycarbonate and polyester and their need for impact  
modification are well known. For example, European Patent Publication  
EP1207172A2 discloses an improved impact modifier for blends of polyester  
20   with other polymers, including polycarbonate, wherein the impact modifier  
itself is a blend of a core/shell additive and a linear copolymer of olefin, alkyl  
acrylate, and glycidyl methacrylate monomers.

Summary of the Invention

25               What is needed is better impact modification for blends of polycarbonate  
(PC) and polyester, especially polyethylene terephthalate (PET) and/or  
polybutylene terephthalate (PBT). There is a need to produce blends which  
have good impact properties, smooth surface finishes, weatherability, scratch  
resistance, solvent resistance, and a balance of flexural modulus, heat distortion  
30   temperature, and impact properties.

The present invention provides use of a thermoplastic vulcanizate (TPV) as a impact modifier that enhances impact properties throughout service temperatures (-40°C to 98°C) for polyester/polycarbonate blends, particularly PC-PET or PC-PBT blends without compromising heat distortion temperature or flexural modulus properties.

The new impact modifier can be used alone, or optionally in combination with one or both of the impact modifiers disclosed in EP1207172A2. The impact modifier is a thermoplastic vulcanizate, which is a blend of a polyolefin and a rubber. The rubber can be fully-crosslinked, partially cross-linked, or dynamically cross-linked during blending of the impact modifier in the thermoplastic polymer.

One aspect of the present invention is a thermoplastic polymer blend, comprising (a) a polyester; (b) a polycarbonate; and (c) a minor amount of a thermoplastic vulcanizate.

"Minor amount" means the amount of thermoplastic vulcanizate in the blend is less than the sum of the amounts of the polyester and the polycarbonate. Preferably, the thermoplastic vulcanizate remains as distinct domains within the thermoplastic polymer blend.

One feature of the blends of the present invention is good impact properties at service temperatures ranging from about -40°C to 98°C without compromising other physical properties otherwise present, e.g., flexural modulus, tensile strength, and heat distortion temperature.

An advantage of the blends of the present invention is that a single compound can be converted into parts that requires service temperatures ranging from about -40°C to 98°C.. In some applications, the parts produced from these blends can be exposed to high temperature at one section of the part and to low temperature at another section without failure. For example, in an exterior automotive application, the same part can function predictably notwithstanding its use in Alaska in the winter and Arizona in the summer.

Moreover, a part designed to be adjacent a heat source can function even in a very cold environment, for example, a snow blower engine housing.

Another advantage of the blends of the present invention is that the blend can be pigmented according to design color choice of the manufacturer  
5 with an excellent surface finish.

Other features and advantages will be revealed in the discussion of the embodiments below.

#### Embodiments of the Invention

##### Thermoplastic Polymers to be Impact Modified

10 The thermoplastic polymers can be a blend of polycarbonate (PC) and polyester (such as polyethylene terephthalate (PET), polypropylene terephthalate (PPT), polybutylene terephthalate (PBT), poly(ethylene-2,6-naphthalate) (PEN), polypropylene naphthalate (PPN), poly(1,4-cyclohexanedimethanol terephthalate) (PCT), polyethylene naphthalate  
15 dibenzoate (PENDB), and polybutylene naphthalate (PBN)).

Additionally, one can add to the blend any of a number of polymers of the polycondensate type including without limitation, and polyester-type of liquid crystalline polymers (LCP).

Of these possibilities, a blend of polycarbonate and a polyester is  
20 desirable with a blend of PC with either PET or PBT being preferred.

The amount of thermoplastic polymer in the blend can range from about 50 to about 95, and preferably from about 60 to about 90 weight percent of the blend.

The relative contribution of the polycarbonate to the blend ranges from  
25 about 15 to about 85 weight percent, and preferably from about 20 to about 70 weight percent of the blend.

The relative contribution of the polyester to the blend ranges from about 15 to about 85 weight percent, and preferably from about 20 to about 70 weight percent of the blend.

30 Thermoplastic Vulcanizate Impact Modifier

Any thermoplastic vulcanizate can be useful in the present invention to the extent that it exhibits compatibility with the polyester and polycarbonate polymers.

Non-limiting examples of commercially available thermoplastic vulcanizates include partially and fully vulcanized TPVs known to one skilled in the art, including Onflex™-V from PolyOne, Santoprene™ from ExxonMobil Chemicals, Sarlink™ from DSM, Nexprene™ and Respond™ from Solvay, and Forprene™ brand thermoplastic vulcanizates from SoFteR SpA.

Of the vulcanized portion of the thermoplastic vulcanizate, ethylene-propylene-diene (EPDM) is preferred because it has one of the lowest glass transition temperatures ( $T_g$ ) available commercially and yet is reasonable in cost.

As stated above, the thermoplastic vulcanizate can be fully cross-linked at the time mixing into the blend or partially cross-linked, or uncross-linked but ready for dynamic vulcanization during melt blending of the polyester and polycarbonate resins.

As stated above, the thermoplastic vulcanizate is present in a minor amount. Desirably, the thermoplastic vulcanizate can be included in the blend of the present invention in an amount from about 3 to about 40, and preferably from about 5 to about 20 weight percent of the blend. Most preferably, the amount is about 7 to about 10 weight percent of the blend.

#### Optional Core/Shell Impact Modifier

The optional impact modifier is comprised of (A) a core/shell additive comprised of core based on alkyl acrylate, on a polyorganosiloxane rubber or a blend thereof and a shell based on poly(alkyl methacrylate), or on a styrene-acrylonitrile copolymer. Preferably the core/shell additive comprises from:

(a) 70% to 90% by weight, of an elastomeric crosslinked core which is comprised of:

1) of 20% to 100% by weight, of a nucleus composed of a

copolymer (I) of n-alkyl acrylate, the alkyl group of which has a carbon number ranging from 5 to 12, and preferably ranging from 5 to 8, or of a mixture of alkyl acrylates, the linear or branched alkyl group of which has a carbon number ranging from 2 to 12, or of a polyorganosiloxane rubber, of a polyfunctional crosslinking agent possessing unsaturated groups in its molecule, at least one of which is of  $\text{CH}_2=\text{C} <$  vinyl type, and optionally of a polyfunctional grafting agent possessing unsaturated groups in its molecule, at least one of which is of  $\text{CH}_2=\text{CH}-\text{CH}_2$  -- allyl type, the said nucleus containing a molar amount of crosslinking agent and optionally of grafting agent ranging from 0.05% to 5% and preferably an amount of between 0.5% and 1.5%; 2) of 80% to 0% by weight of a covering composed of a copolymer (II) of n-alkyl acrylate, the alkyl group of which has a carbon number ranging from 4 to 12, or of a mixture of alkyl acrylates as defined above in 1) and of a polyfunctional grafting agent possessing unsaturated groups in its molecule, at least one of which is of  $\text{CH}_2=\text{CH}-\text{CH}_2$  -- allyl type, the said covering containing a molar amount of grafting agent ranging from 0.05% to 2.5%; (b) 30% to 10% by weight, of a shell grafted onto the said core composed of a polymer of an alkyl methacrylate, the alkyl group of which has a carbon number ranging from 1 to 4, or alternatively of a statistical copolymer of an  $\text{<DP}=2$  alkyl methacrylate, the alkyl group of which has a carbon number ranging from 1 to 4, and of an alkyl acrylate, the alkyl group of which has a carbon number ranging from 1 to 8, containing a molar amount of alkyl acrylate ranging from 5% to 40%, or alternatively composed of a styrene-acrylonitrile copolymer having a preferred styrene:acrylonitrile molar ratio between 1:1 and 4:1, and particularly between 7:3 and 3:1, respectively; wherein optionally 0.1 to 50 weight percent of vinyl monomers have functional groups.

Such core/shell impact modifiers are commercially available such as the n-octyl acrylate rubber core/polymethylmethacrylate shell product commercially available as "D-400" from Atofina Chemicals, Inc. of Philadelphia, PA.

Such core/shell impact modifier can be included in the blend of the present invention in an amount from about 0 to about 10, and preferably from about 0 to about 7. Most preferably, the amount is about 1 to about 5 percent by weight of the blend.

5           Optional Linear Terpolymer Impact Modifier

This optional impact modifier comprises a linear terpolymer of (a) ethylene, (b) a lower alkyl acrylate and (c) a monomer which contains a heterocycle containing one oxygen atom as the hetero-atom.

10           "Lower alkyl acrylate" means a C<sub>1</sub>-C<sub>8</sub> and preferably a C<sub>1</sub>-C<sub>4</sub> alkyl ester of (meth)acrylic acid. Of these possibilities, methyl acrylate is preferred.

            Preferably the heterocyclic monomer contains an epoxy atom.

            Relative amounts of monomer in the terpolymer range from 55-75 weight percent ethylene, 20-30 weight percent lower alkyl acrylate, and 5-15 weight percent heterocyclic monomer.

15           Such linear terpolymer impact modifiers are commercially available such as the ethylene-methyl acrylate-glycidyl methacrylate product commercially available as "Lotader AX 8900" from Atofina Chemicals, Inc. of Philadelphia, PA.

            Such linear terpolymer impact modifier can be included in the blend of  
20           the present invention in an amount from about 0 to about 10, and preferably from about 0 to about 7. Most preferably, the amount is about 1 to about 5 percent by weight of the blend.

            Each of the three impact modifiers can be in powder, flake, or pellet form. They can be blended together into a concentrate or mixed with the  
25           thermoplastic polymers during melt processing in preparation for direct molding or pelletization for later molding.

Optional Additives

            As with many thermoplastic compounds, it is optional and desirable to include other additives to improve processing or performance. Non-limiting  
30           examples of such optional additives include slip agents, antiblocking agents,

antioxidants, ultraviolet light stabilizers, quenchers, dyes and pigments, plasticizers, mold release agents, lubricants, antistatic agents, fire retardants, and fillers such as glass fibers, talc, chalk, or clay. Of these fillers, the properties of nanoclay can add stiffness, toughness, and charring properties for flame retardancy.

Such optional additives can be included in the blend of the present invention in an amount from about 0 to about 40, and preferably from about 0.1 to about 30 weight percent. Most preferably, the amount is about 0.5 to about 10 weight percent of the blend.

#### 10        Method of Processing Blends

The blend of the present invention can be prepared by any method which makes it possible to produce a thoroughly mixed blend containing the polycarbonate, the polyester, and the thermoplastic vulcanizate impact modifier along with any optional impact modifiers described above, and other optional additives, if any. It is possible, for example, to dry-mix the ingredients constituting the compound, then to extrude the resulting mixture and to reduce the extrudate to pellets.

As an example, extrusion can be carried out in a suitable extruder, such as a Werner-Pfleiderer co-rotating twin screw extruder. The extruder should be capable of screw speeds ranging from about 10 to about 2000 rpm, preferably from about 50 rpm to 1500 rpm. The temperature profile from the barrel number two to the die should range from about 170°C to about 350°C, and preferably from about 220°C to about 270°C so as to extrude at the processing temperature of the components of the desired compound. The extruder can be fed separately with the ingredients of the blend or together.

The selected temperature range should be from about 200°C to about 260°C for a PC/PBT based blend or a PC/PET based blend. The extrudate can be pelletized or directed into a profile die. If pelletized, the pellets can then be

converted to an article by injection molding, compression molding, blow molding or other techniques known to those skilled in the art.

Preferably, one can introduce the polycarbonate and the polyester in split feed streams in two different ports of the extruder (main throat and down stream locations) with the use of both atmospheric vents and vacuum vents as  
5 preferred by those skilled in the art. High specific energy input is desirable to reduce the size of the impact modifier particles and to encourage uniform dispersion in the thermoplastic polymers. One can use a temperature profile of between 200 and 260°C, depending on the number and type of optional  
10 additives also included in the extruded blend. It is optional to dry the components prior to compounding, depending on the performance properties of final product.

The thermoplastic vulcanizate can be added in its final form or produced *in situ* during the extrusion compounding of the blends of this invention. If  
15 dynamic vulcanization of the thermoplastic vulcanizate is to occur during melt blending, then the following additional items are required or recommended: The uncured PP-EPDM-oil blend is added along with a suitable crosslinking agent, which can include sulphur or its compounds, a peroxide with or without a co-agent, a phenolic resole resin with or without a catalyst activator like an acid  
20 or a Lewis acid or a proton donor, or other means known to one skilled in the art.

#### Usefulness of the Invention

Impact-modified thermoplastic polymer blends of the present invention are useful for transportation-related molded items (e.g., crash helmets and parts  
25 for vehicles such as bumpers and fenders); electrical equipment when flame retardants or reinforcing fillers are also added (e.g., plugs, connectors, boxes, and switches); and consumer appliance housings and containers (e.g., kitchen appliance housings and shells, and consumer electronics housings and cases).

Further embodiments of the invention are described in the following Examples.

### Examples

#### Comparative Example A

5           A mixture of 27.98% of a polybutylene terephthalate (Crestin™ 610 from DuPont), 2.41% of Durastrength™ 400 (a core-shell acrylic-based impact modifier from Atofina), 4.82% of a compatibilizer (Lotader™ AX8900 from Atofina), 0.96% of an antioxidant (Ultranox™ 626 (from GE Specialty Chemicals, now from Crompton Corp.) , 0.32% of an antioxidant (Irganox™ 1010 from Ciba Specialties), 0.21% of an antioxidant (Mark™ 135A from Crompton Corp.) , 0.21% of a thioether stabilizer (Naugard™ 412S from Crompton Corp.) and 1.59% of a lubricant (AC540™ from Honeywell) was dry blended and fed into the main feed of a 44L/D 25 mm. twin screw extruder and another blend of 59.09% of a reprocessed polycarbonate and 2.41% of 15 Durastrength™ 400 was fed in a side feeder downstream into the melt. For Example 1, the process temperatures were set at 402, 452, 452, 476, 450, 469, 431, and 424°F (205°C-233°C-233°C-247°C-232°C-243°C-222°C-218°C) on the various zones on the extruder barrel, 453°F (234°C) at the die with a feed rate of 30 lb./hr. (13.6 kg/hr) at 900 rpm. This resulted in a die pressure of 169 20 psi (1.165 mPa) and a torque of 69%. A vacuum of 20 in. (50.8 cm) was used at the vent to deal with any possible volatiles. The strands from the strand die were fed through a water bath into a pelletizer and the products pelletized. The pellets were subsequently injection molded into the various required test specimens on a Nissei injection molding machine operating at 250°C (T-melt).

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#### Example 1

A blend of 43.08% of a polybutylene terephthalate (PBT 610 from DuPont), 0.96% of Elvaloy PTW (an ethylene- n-butyl acrylate-gycidyl methacrylate compatibilizer from Du Pont), 1.48% of another compatibilizer

(Interloy 1095 from Crompton Corp.), 7.18% of a partially crosslinked TPV, 0.95% of an antioxidant (Ultranox 626 (from GE Specialty Chemicals), 0.31% of an antioxidant (Irganox 1010 from Ciba Specialties), 0.21% of an antioxidant (Mark 135A from Crompton Corp.), 0.21% of a thioether stabilizer (412S from Crompton Corp.) and 1.58% of a lubricant (AC540 from Honeywell) were dry  
5 blended and fed into the main feed of a 44L/D 25 mm. twin screw extruder and another blend of 43.08% of a reprocessed polycarbonate and 0.96% of D-400 were fed in a side feeder downstream into the melt.

The partially crosslinked TPV had been made in two steps. In the first  
10 step a masterbatch was prepared in a Banbury with 3.225 lb. of an oil-extended EPDM (Buna EP G 3569 from Bayer), 0.417 lb. of a 0.5 MFR polypropylene homopolymer (Pro-fax PDC 1272 from Basell), 0.045 lb. of a 10-14 MFR polypropylene homopolymer, 0.910 lb. of a reactor TPO based on propylene and ethylene (Hifax CA10A from Basell), 1.445 lb. of a paraffinic oil (6001R  
15 from Chevron-Texaco), 0.730 lb. of a 12 MFR polypropylene (Pro-fax PH6331NW from Basell), 0.730 lb. of a talc (Cimpack 610 from Luzenac America), 0.161 lb. of zinc oxide (Kadox 915 from Zinc Corp.), 0.010 lb. of zinc stearate (from Witco Division of Crompton Corp.), 0.010 lb. of calcium stearate (from Crompton Corp.), 0.010 lb. of stearic acid (Emersol 132 from  
20 ChemCentral Corp. ), 0.005 lb. of an antioxidant (Irganox 1010 from Ciba Specialties, 0.005 lb. of another antioxidant (Ultranox 626 from Crompton), 0.005 lb. of another antioxidant (Anox 18 from Great Lakes Chemicals), 0.005 lb. of a phosphite stabilizer (Irgafos 168 from Ciba Specialties) and 0.030 lb. of titanium dioxide (RCL-188 from Tiona). Microthene 709FA was used as a  
25 dusting agent to make sure that the masterbatch pellets did not agglomerate after the molten mix from the Banbury was conveyed to a rubber roll mill set at 280°F (138°C) and then the sheets from the roll mill were diced on a dicer into pellets. These masterbatch pellets were further compounded in a second step into a partially vulcanized TPV using the following formulation on a 25 mm.

44L/D twin screw extruder manufactured by Werner-Pfleiderer (now called Coperion). A pellet blend of 88.0% masterbatch from above, 7.0% of the same 12 MFR PP used above, and 0.1% of the same titanium dioxide used above were fed into the main hopper while 4.9% of a molten mixture, made from 36%  
5 of a phenolic resole resin (SP1045 from Schenectady Chemicals) and 64% of the same paraffin oil used above, was injected hot at 150°C into the twin screw down stream into the melt. Due to low residence times and insufficient co-catalyst, the TPV formed was partially crosslinked with a mostly EPDM-oil continuous phase. This partially crosslinked TPV was used as the impact  
10 modifier in the subsequent step to make the impact modified engineering plastic with polycarbonate-polyester alloy.

The process temperatures for this step were: 408, 452, 452, 477, 460, 472, 424, and 418°F (205°C-233°C-233°C-247°C-237°C-244°C-218°C-214°C) on the various zones on the extruder barrel, 453°F (234°C) at the die with a feed  
15 rate of 30 lb./hr. (13.6 kg/hr) at 900 rpm. This resulted in a die pressure of 160 psi (1.103 mPa) and a torque of 35%. A vacuum of 18 in. (45.7 cm) was used at the vent to deal with any possible volatiles. The strands from the strand die were fed through a water bath into a pelletizer and the products pelletized. The pellets were subsequently injection molded into the various required test  
20 specimens on a Nissei injection molding machine operating at 250°C (T-melt).

### Example 2

A blend of 43.03% of a polybutylene terephthalate (PBT 610 from DuPont), 0.96% of Elvaloy PTW (an ethylene- n-butyl acrylate-glycidyl  
25 methacrylate compatibilizer from Du Pont), 1.58% of another compatibilizer (Interloy 1095 from Crompton Corp.), 7.17% of a partially crosslinked TPV, 0.95% of an antioxidant (Ultrinox 626 (from GE Specialty Chemicals) , 0.32% of an antioxidant (Irganox 1010 from Ciba Specialties), 0.21% of an antioxidant (Mark 135A from Crompton Corp.) , 0.21% of a thioether stabilizer (412S from

Crompton Corp.) and 1.58% of a lubricant (AC540 from Honeywell) were dry blended and fed into the main feed of a 44L/D 25 mm. twin screw extruder and another blend of 43.03% of a reprocessed polycarbonate and 0.96% of D-400 were fed in a side feeder downstream into the melt.

- 5           The partially crosslinked TPV had been made in two steps. In the first step, a masterbatch was prepared in a Banbury with 46.08 parts of Buna EP G3569, 5.06 parts of Pro-fax PDC1272, 0.64% of Pro-fax PH6331NW, 12.88 parts of Hifax CA10A, 10.43 parts of Cimpact 610, 2.3 parts of zinc oxide, 0.14 parts of zinc Stearate, 0.14 parts of calcium stearate, 0.14 parts of stearic acid, 10   0.005 parts of Irganox 1010, 0.005 parts of Ultranox 626, 0.005 parts of Anox 18, 0.005 parts of Irgafos 168, 0.43 parts of titanium dioxide, and 20.63 parts of Hydrobrite 550 PO Oil, where all the ingredients used were from the same sources as those listed in Example 1. Microthene 709FA was used as a dusting agent to make sure that the masterbatch pellets did not agglomerate after the 15   molten mix from the Banbury was conveyed to a rubber roll mill set at 280°F (138°C) and then the sheets from the roll mill were diced on a dicer into pellets. These masterbatch pellets were further compounded in a second step into a partially vulcanized TPV using the following formulation on a 25 mm. 44L/D twin screw extruder manufactured by Werner-Pfleiderer (now called Coperion).
- 20           A pellet blend of 88.0 parts masterbatch from above, 6.0 parts of the same 0.5 MFR PP used above, and 0.11 parts of the same titanium dioxide used above were fed into the main hopper along with 0.33 parts of Lowilite 26, a UV stabilizer from Great Lakes Chemicals, 0.33 parts of Lowilite 55, a phosphite stabilizer from Great Lakes Chemicals, 0.33 parts of Anox 20, an antioxidant 25   from Great Lakes Chemicals, and 1.5 parts of SP 1055 Brominated Phenolic Resole Resin from Schenectady Chemicals. Hydrobrite 550 PO, a paraffin oil was injected into the twin screw down stream into the melt, at a ratio of 3.1:96.9 parts of the total mixture fed in the main hopper. Due to low residence times

and insufficient co-catalyst, the TPV formed was partially crosslinked with a predominantly EPDM-oil continuous phase.

This partially crosslinked TPV was used as the impact modifier in the subsequent step to make the impact modified engineering plastic with polycarbonate-polyester alloy. The process temperatures for this step were: 408, 452, 452, 477, 460, 472, 424, and 418°F (205°C-233°C-233°C-247°C-237°C-244°C-218°C-214°C) on the various zones on the extruder barrel, 453°F (234°C) at the die with a feed rate of 30 lb./hr. (13.6 kg/hr) at 900 rpm. This resulted in a die pressure of 160 psi (1.103 mPa) and a torque of 35%. A vacuum of 18 in. (45.7 cm) was used at the vent to deal with any possible volatiles. The strands from the strand die were fed through a water bath into a pelletizer and the products pelletized. The pellets were subsequently injection molded into the various required test specimens on a Nissei injection molding machine operating at 250°C (T-melt). Table 1 summarizes the formulations for Examples 1-3 and order of addition.

Table 1				
Recipes in parts		Comparative Example A	Example 1	Example 2
Fed at Throat:				
Raw Materials	Supplier			
PBT-610	Du Pont	27.98%	43.08%	43.03%
Durastrength 400	Atofina	2.41%	--	--
Lotader AX 8900	Atofina	4.82%	--	--
Elvaloy PTW	DuPont	--	0.96%	0.96%
Interloy 1095	Crompton Corp.	--	1.48%	1.58%
TPV (partially crosslinked made from EPDM, PP and oil)	PolyOne		7.18%	7.17%
Ultranox 626	Crompton Corp	0.96%	0.95%	0.95%
Irganox 1010	Crompton Corp	0.32%	0.31%	0.32%
Mark 135A	Crompton Corp	0.21%	0.21%	0.21%
Naugard 412S	Crompton Corp	0.21%	0.21%	0.21%
AC 540	Honeywell	1.59%	1.58%	1.58%
Following items feed downstream:				
Repro-PC	Commercial Recycling Co.	59.09%	43.08%	43.03%
D-400	Atofina	2.41%	0.96%	0.96%

### Examples 3-5

The composition from Example 2 was further compounded with glass fiber and/or nanoclay using the formulations in Table 2:

Table 2			
Component	Example 3	Example 4	Example 5
Pellets from Example 2	68%	90%	70%
Glass fiber	32%	0%	20%
Nanoblend™ 3100 nanoclay concentrate (PolyOne)	0%	10%	10%

The pellets from Example 2 were dried and then fed into the main feed hopper of a 25 mm 44 L/D extruder described in Comparative Example A with the same conditions described in Example 1. In the case of Examples 4 and 5, a masterbatch prepared from Nanoblend™ nanoclay concentrate, a nanoclay masterbatch in an ethylene-methyl acrylate copolymer, was fed into the main hopper along with the pellets prepared and described in Example 2. This resulted in a die pressure of 300, 150 and 310 psi, respectively, (2.068, 1.034, and 2.137 mPa, respectively) and a torque of 65%, 35% and 66%, respectively. A vacuum of about 20 in. (50.8 cm) was used at the vent to deal with any possible volatiles. The strands from the strand die were fed through a water bath into a pelletizer and the products pelletized. The pellets were subsequently injection molded into the various required test specimens on a Nissei injection molding machine operating at 250°C (T-melt). The specimens from these three examples also showed excellent surface appearance and superior flexural modulus compared to those prepared from the Comparative Example A as well as those prepared in Examples 1 and 2.

#### Test Methods

Table 3 shows the test methods used in conjunction with the evaluation of the examples.

Table 3	
Test Name	Test Method
Heat Distortion	ASTM D648 (@ 66psi and 264 psi)
Tensile Strength	ASTM D638

Table 3	
Test Name	Test Method
Flexural Modulus	ASTM D790
Notched Izod Impact Strength	ASTM D256
% Elongation at Break	ASTM D638 Rigid
Surface Appearance	Visual Rating

### Results

Table 4 shows the experimental results from Comparative Examples A  
5 and Example 1.

Table 4			
Test		Comparative Example A	Example 1
Heat Distortion (°C) with 66 psi Distortion	Trial 1	92	100
	Trial 2	95	100
	Average	93.5	100
Heat Distortion (°C) with 264 psi Distortion	Trial 1	79	77
	Trial 2	79	78
	Average	79	77.5
Stress at Yield (psi)		7446	7764
Stress at Break (psi)		6340	5920
Flexural Modulus (psi x 1000)		325.4	339.4
Average Impact (ft*lb/in) @ 23°C		15.35	12.48
Average Impact (ft*lb/in) @ -20°C		3.58	2.24
Average Impact (ft*lb/in) @ -40°C		2.92	2.06
Elongation Strain at Break (%)		110	34
Surface Appearance		Moderately Attractive	Excellent

Table 3 shows that Example 1 outperforms Comparative Example A  
even though it had 15% less total impact modifier (8.1% vs. 9.6%). Example 1  
had better flexural modulus and tensile strength at yield than Comparative  
10 Example A.

The invention is not limited to the above embodiments. The claims  
follow.